40 CFR Part 60, Subpart Ja - Requirements Reference Tables

Subpart Ja Standards

- §60.102a(b)(1)(i)|1 PM requirements in wt PM per wt coke burn-off for modified or reconstructed FCCUs
- §60.102a(b)(1)(i)|2 PM requirements in gr/dscf for modified or reconstructed FCCUs
- §60.102a(b)(1)(ii)|1 PM requirements in wt PM per wt coke burn-off for newly constructed FCCUs
- §60.102a(b)(1)(ii)|2 PM requirements in gr/dscf for newly constructed FCCUs
- §60.102a(b)(1)(iii)|1 PM requirements in wt PM per wt coke burn-off for FCUs
- §60.102a(b)(1)(iii)|2 PM requirements in gr/dscf for FCUs
- §60.102a(b)(2) NO_X requirements for FCCUs and FCUs
- §60.102a(b)(3) SO₂ requirements for FCCUs and FCUs
- §60.102a(b)(4) CO requirements for FCCUs and FCUs
- §60.102a(d) PM (Opacity) requirements for FCCUs and FCUs using cyclones
- §60.102a(f)(1)(i)|1 SO₂ requirements for sulfur recovery plants greater than 20 LTD with an oxidation control or a reduction control system followed by incineration using Equation 1
- §60.102a(f)(1)(i)|2 SO₂ requirements for sulfur recovery plants greater than 20 LTD with an oxidation control or a reduction control system followed by incineration on an SO₂ ppmv basis
- §60.102a(f)(1)(ii)|1 SO₂ requirements for sulfur recovery plants greater than 20 LTD with a reduction control system not followed by incineration using Equation 1
- §60.102a(f)(1)(ii)|2 SO₂ requirements for sulfur recovery plants greater than 20 LTD with a reduction control system not followed by incineration on an SO₂ ppmv basis
- §60.102a(f)(1)(iii) H₂S requirements for sulfur recovery plants greater than 20 LTD with a reduction control system not followed by incineration
- §60.102a(f)(2)(i)|1 SO₂ requirements for sulfur recovery plants equal to or less than 20 LTD with an oxidation control or a reduction control system followed by incineration using Equation 2
- §60.102a(f)(2)(i)|2 SO₂ requirements for sulfur recovery plants equal to or less than 20 LTD with an oxidation control or a reduction control system followed by incineration on an SO₂ ppmv basis
- §60.102a(f)(2)(ii)|1 SO₂ requirements for sulfur recovery plants equal to or less than 20 LTD with a reduction control system not followed by incineration using Equation 2
- §60.102a(f)(2)(ii)|2 SO₂ requirements for sulfur recovery plants equal to or less than 20 LTD with a reduction control system not followed by incineration on an SO₂ ppmv basis
- §60.102a(f)(2)(iii) H₂S requirements for sulfur recovery plants equal to or less than 20 LTD with a reduction control system not followed by incineration
- §60.102a(g)(1)(i) SO₂ requirements in ppmv emitted SO₂ for fuel gas combustion devices
- §60.102a(g)(1)(ii) H₂S requirements in ppmv H₂S content of fuel gas for fuel gas combustion devices
- §60.102a(g)(1)(iii) exemption for combustion in a portable generator of fuel gas released as a result of tank degreasing and/or cleaning
- §60.102a(g)(2)(i)(A) NO_X requirements for natural draft process heaters with a rated capacity greater than 40 MMBtu/hr used as a fuel gas combustion device on a ppmv basis
- §60.102a(g)(2)(i)(B) NO_X requirements for natural draft process heaters with a rated capacity greater than 40 MMBtu/hr used as a fuel gas combustion device on a lb/MMBTU basis

- §60.102a(g)(2)(ii)(A) NO_X requirements for forced draft process heaters with a rated capacity greater than 40 MMBtu/hr used as a fuel gas combustion device on a ppmv basis
- §60.102a(g)(2)(ii)(B) NO_X requirements for forced draft process heaters with a rated capacity greater than 40 MMBtu/hr used as a fuel gas combustion device on a lb/MMBTU basis
- §60.102a(g)(2)(iii)(A) NO_X requirements for co-fired natural draft process heaters with a rated capacity greater than 40 MMBtu/hr used as a fuel gas combustion device on a ppmv basis
- §60.102a(g)(2)(iii)(B) NO_X requirements for co-fired natural draft process heaters with a rated capacity greater than 40 MMBtu/hr used as a fuel gas combustion device using Equation 3
- §60.102a(g)(2)(iv)(A) NO_X requirements for co-fired forced draft process heaters with a rated capacity greater than 40 MMBtu/hr used as a fuel gas combustion device on a ppmv basis
- <u>§60.102a(g)(2)(iv)(B)</u> NO_X requirements for co-fired forced draft process heaters with a rated capacity greater than 40 MMBtu/hr used as a fuel gas combustion device using Equation 4
- §60.102a(i) alternative requirements for process heaters that meet the criteria
- §60.103a(h) H₂S requirements for any affected flare used as a fuel gas combustion device
- §60.103a(i) work practice standard for delayed coking units
- §60.103a(j)(1)|1 alternative means of emission limitation for SO₂
- §60.103a(j)(1)|2 alternative means of emission limitation for H₂S

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